CAD OF PROCESSES FOR SILICON HIGH SPEED DEVICES

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ABSTRACT

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INTRODUCTION

In the ideal situation process modeling should support accurate, predictive simulation of advanced technologies. If this were true, then the majority of the development of new technologies would be accomplished via simulators and the time required for such development could be dramatically abbreviated

It is widely believed that process simulation of advanced processes will res-cue the semiconductor industry from the prohibitive costs of developing and optimizing such processes experimentally. Our experience shows us that reality is different. It is the goal of this work clarify some issues connected with this topic

Because most commercially available process simulation tools are prepared by the software houses, the using of these tools is so simple that almost everybody has immediate confidence in designing of fabrication processes using the computer, in the beginning of these activities the engineers often discover that the result are not even close to the experimental data. They conclude that CAD process modeling is either useless in the worst case or they try to discover the principle of the used models and localize the source of error in the best case. The conclusions from both groups, lead to a final statement that our knowledge of physics and chemistry of majority processes does not allow us to built process simulation tools which can be used for complex simulation of submicron VLSI fabri-cation processes.

One can find many reasons for this situation. One is that the modeling theory can not precede (except in a few applications) the progress in equipment used in the pro-duction of VLSI technologies. Additional reasons are related to the work of designers of TCAD tools and they are:

- -lack of systematic approach in used theory
- -poor knowledge of state of the art processing
- Hack of discipline with regard to the experimental data

The combination of these and other factors raises many questions. The main questions addressed here are; is process modeling useless ? Where are the main benefits if the answer to the first question is no ? Even if there are serious limitations how we can maximize utilization for the design of submicron processes ?

Our experience show us that process simulation is a very useful complement of experimental work during designing of the new tabrication processes and a major benefit which can be expected from sophisticated (and we must emphasize this point) process modeling is increased probability of first pass success on a new process. In the following section, we shall first discuss the details of device shrinking and consequent changes in processing, followed by a presentation of the concentration profile engineering where we will manifest the major deticiencies in TCAD. Finally, we shall consider an example application modeling the submicron structure.

DEVICE SHRINKING AND CONSEQUENT CHANGES IN PROCESSING

To illustrate the type of requirements imposed by technological processing on modeling capabilities of TCAD tools we compare three processes which were developed in the same facility during the last decade. All processes are designed for ECL type of circuits.

From the Table I, one can make the following conclusions

- -The most dramatic increases of processing steps is in reactive ion etching and LPCVD polysilicon depositions. Both processes are charactenzed by high level of contamination.
- Very significant increase can be seen also for Rapid Thermal Annealing
- steps. - All devices in new technologies are built on epitaxial silicon with a very
- low oxygen concentration. An inevitable and yet commonality of all the process steps that are increasing in frequency

most rapidly in advanced technologies is the production of damage of the crystal lattice with production of native defects and contamination by deep impurities

The native defects (vacancy, self interstitial, interstitial) are believed to play a dominant role in diffusion of impurities and in determining the electrical properties of semiconductor mate-Indiaison of impunities and in tootomining on implantation (with damago of the structure atter implantation) is often discussed in recent likerature and several models have been pro-posed to explain these phenomena (11). Intuitively we can expect some anomalies in the redistribution of impurities. However, Misra and Haseli (2) show that even in RIE process-ing where the water temporature goes up to 300 °C (as a function of RF power density) this importance is official to individe the difference of antion event difference and here the temporature is sufficient to induce the diffusion of native point detects and therefore change the diffusion behavior. But the annealing behavior of RIE induced defects are rela-tively unknown. The situation is similar for RTA processes. These circumstances result in a very poor basis for the creating of models for TCAD.

Another very important conclusion can be deduced from Table I. The next generation of tochnological processes will extensively use single water processing equip-ment where there is no possibility for monitor waters. Therefore we cannot (unless we add

an additional (est structure) verify the results and reproducibility of processing. This point has very important consequences for the acquisition of experimental data which we need for the design of models appropriate for TCAD. Generally the data can be extracted from the special objects where processing conditions could be slightly or significantly different than the process conditions on the structure which is under investigation

CONCENTRATION PROFILE ENGINEERING

The typical approach of developing new tablication processes usually assumes that we know target concentration profiles for the devices. The target profile of de-vices is determined by a variety of approaches: intuitively, based on our previous expenences or as a result of relatively predictable device simulations. Profile engineering is a process of designing of individual technological operations in such a way that we can create the desired structure and at the same time meet the requirements defined by the target prohia.

The process steps used in VLSI fabrication technologies can be divided into three modules. Every module is typically formed of the following substructures:

- -solation structure and bulk of active devices
- -active devices

-interconnections and contact

Each module has a unique position in the process flow and is characterized by range of processing temperatures. Fig. 1 shows a simplified diagram of processing temperatures and times for three processes which we mentioned earlier. For example, process M5 is 100 minutes in a range of tomperatures higher than 1000°C, 855 minutes in a range of tempera-tures between 900°C and 1000°C and 120 minutes at temperatures between 800°C and 900°C. Surprisingly and contrary to common myth, the thermal budget of advanced pro-cesses is not lower than "conventional" (not submicron) processes. The time of processing with temperatures higher than 1000°C is decreasing, but the total time of thermal process-ing is longer. If we introduce the performance index as product of the processing time and the processing time to processing time and the performance index as product of the processing time and the processing temperature we can find:

process	performance index [°C min]
MI	550E3
M3	890E3
M5	960E3

From the viewpoint of diffusion and redistribution of impurities, this does not mean a trend in the wrong direction because the main part of the higher thermal budget is for the more complicated isolation structure. If we compare the same performance index for steps after deep collector formation:

BJT 1952 ECL LOCOS 2 2500	8JT 1986 ECL LOCOS 175 1200	BICMOS 1990 ECL TRENCH 1 2 900
1982 ECL LOCOS 2 2500	1986 ECL LOCOS 1 75 1200	1990 ECL TRENCH 1 2 900
ECL LOCOS 2 2500	ECL LOCOS 1 75 1200	ECL TRENCH 1 2 900
2 2 2500	LOCOS 1 75 1200	TRENCH 1 2 900
2 2500	1 75	1 2 900
2500	1200	900
14	16	20
7	7	15
0	12	25
0	0	0
1	0	0
3	5	6
1	1	з
0	1	5
3	6	7
0	з	7
2	4	4
0	4	0
1	1	3
0	- , -	2
0	1	1 1
'	1	
33	63	107
	14 7 0 0 1 3 0 3 	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$

Table I, Comparison of processes M1,M2 M3

- NOTES 1 process M1 uses implanted emitter 2 process M3 and M5 use a polysilicon emitter 3 A5 processes are settaigment processes 4 in M1 deep collector follow the baselennitifor formation 5 Number of implantation steps in M5 include the timushold and punchthrough implants

process	pertormance index (°C min)	
MI	74E3	
M3	110E3	
M5	13563	

In all cases, after formation of the isolation and wells we have a concentration profile which is exposed to thermal treatment shorter than 120 minutes. This treatment has a small impact on the bulk concentration profile. This is illustrated in Fig. 2 and Fig. 3 where the changes after the projected thermal budget for typical processing of an active device (+ e.gate source/drain base, emitter) at 950°C are shown for the NPN and N—channel transister respectively. From both plots it is clear that the changes in redistribution of impurities are very small.

THE MAJOR DEFICIENCIES IN PROCESS MODELING

Before we go further in our discussion we need to clarify questions regarding the dimensionality of process simulation tools. The typical opinion is that submicron devices necessitate two-dimensional process simulation. In our view the major problems where lateral diffusion is important can be solved in one dimension with appropriate interpolation into the second dimension. Where two dimensional solutions are needed is for diffusion into the second dimension (as is polysilicon with a columnar structure). In Fig.4 and Fig.5 a comparison is shown between boron diffusion from polysilicon in two structures with an oxidd/nitride window. The interface area between the polysilicon and silicon is the same in both cases. From calculated data we can see that the error in purching hedge to the polysilicon, leads to a poor prediction of emitter junction depit. This is true where arsenic is implanted into nonplanar polysilicon and diffuses into solicon through a tapered oxide spacer window with a vory big aspect ratio w_{bo}/w_{bottom}.

The difficulties accompanying process modeling are very well know; for a general review of this issues see for example [3]. If we focus only on diffusion modeling then the main deficiencies can be listed as:

-Diffusion principle is not defined.

 Vacancies are considered to promote diffusion by formation of defectimpunity pairs, but the process of formation of pairs is not explicitly in-

cluded.

- -Nonequilibrium phenomena are not included.
- -Annealing of point defects is not included.
- The contribution of individual point defect or defect-impurity pairs to diffusion is not known.
- -No diffusivity dependence on heating and cooling rates are accounted for
- –No dependence of diffusion behavior on the thermal history of the wafer is included.
- -An inconsistency in low and high temperature diffusion behavior

Our expenence shows us that there is another source of difficulties which is not very often remembered – immense discrepancies between active and chemical concentration (especially if RTA is used in processing) as will be shown in our comparison of activation efficiency by RTA compared to a conventional fumace anneal.

In all commonly available process modeling programs, basic phenomenological diffusion models are used, After many years of application they have been rolatively well "calibrated" (fitted) to a large class of equilibrium diffusion problems. Unfortunately, these ciffusion models fail in some increasingly important cases such as diffusion at high concentration, diffusion at low tomperature (reverse annealing or deactivation), redistribution of inpurities from diffusion sources with very steep concentration gradients or diffusion during rapid thermal (RTA) processing. The acquisition of concentration profiles from experiments to "calibrate" the models depends on one or more analytical techniques: SIMS, RBS, incremental Hall and sheet resistance measurement. CV profiling and spreading resistance measurement and and sheet resistance measurement. CV profiling and spreading resistance measurement and use to a large uncertainty in the dotermination of the diffusion coefficient. This is why the analytical data used for "calibration" of these models has been primarily based on the othermical concentration of imputies due to the good accuracy of SIMS However, the electricatity active concentrations are of primary inferest.

Two experiments were conducted to investigate aronic diffusion during RTA. In the first, we have measured enomical and active concentration profile, for samples annealed under similar conditions in the RTA equipment (PEAK ALP 6000) and furnace (TYLAN). The substrates used in this exponment were all 100 mm diameter <1005, CZ, silicon waters of resistivity 6.0–8.5 Qcm, boron doped. One group of waters was thermally exided to an exide thickness of 40nm, LPCVD polysticon of thickness. B80nm was deposited on the second group of waters atter an HF etch. Arsenic with a dose of 1E16 cm⁻² and an energy of 50 keV was implanted into both group of waters. Annealing was performed in a nitrogen ambient with the temporature-time profile shown in Fig.6. The intention was to create the same thermal cycle in both the RTA and furnace anneats. SIMS and SRP wire used to determine the concentration profiles over though the chemical profiles were observed in the active concentration profiles wore the same to find a word of the anneal profiles and the area. SimS and SRP wire used to determinate or the cooling rate of all waters in these experiments. For samples annealed in the RTA system the cooling rate of all waters in these experiments. For samples annealed in the RTA system the cooling rate of all waters in these experiments. For samples annealed in the furnace and cooled in free air, the cooling rate in the same range of C/sec.

In the second experiment, the role of temperature ramp rate during RTA was further explored. The experiment was performed on the same type of samples with a 0 mithock thermatoxide and an arsenic implant of 1E 16 [cm⁻²] at 50keV. The first group was heated up with a "slow" programmed heating rate of 0.333 °C/sec and cooled down with a "last" programmed rate of 4.75 °C/sec. The relative ramp rates for the second group of waters reversed, keeping the time at temperature for the isothermal portion of the annotal (10sec at 950°) and the total thormal budget the same (see Fig.9). SIMS and differential that last encounter at one destruction and mobility were used for acquisition of chemical and electrically active concentration profiles, respectively. As seen from the measurement of carrier concentration as approximatuly 150 times greater than the respectively 150 times greater

the "slow" cooling rate, gave an active concentration that was only 2 times higher. We can conclude that the faster cooling rate in the RTA anneal can contribute to higher activation efficiency, but another variable is clearly responsible for the majority of the effect. The experiments described above were not simulated correctly by using process simula-

The experiments described above were not simulated correctly by using process simulation tools.

Many of the problems listed above can be solved (or at least improved) by correct determination of the Form level of the diffusion system and appropriate dependence of diffusivity on concentration of point defects. A reliationship which describes the concentration of point defects in the form i/n, ¹ does not follow the temperature dependence of the point defects, the dependence of the point defects, the dependence of diffusivity as a function of doing concentration to its approximation does not lead to "saturation" of the concentration of point defects. Also, the relative changes of concentration of individual charged defects with doping level are independent of activation energy. However, it is known from the behavior of degenerate semiconductors that, in the limit, further increases in impunty concentration cannot increase the concentration of point defects.

ADVANCED MODEL FOR IMPURITY DIFFUSION IN SILICON

Several new models for modeling of diffusion processes including RTA have been developed recently [4]. However, these approaches use a physical formalism which has the same deficiencies mentioned above, and are improved only in that a higher number of litting parameters in the diffusion coefficient allow for higher degree of freedom in calibration.

We extended the previous work on the point delect diffusion mechanism in silicon and propose an improved version of the diffusion model. We solve for the Fermi dovit and eliminate contain ideas facking acceptable physical background, for example the fractional interstitial factor fi. The relative importance of each mechanism depends on the time evolution of all species present in the system This model is described by the following equations:

$$\frac{\partial [A_{IJ}]}{\partial t} = k_{i}^{-}[A_{I}] - k_{i}^{*}[A_{J}][I] + k_{v}^{-}[A_{J}][V] - k_{v}^{*}[A_{J}] - k_{A,V}^{*}[A_{J}][V] + k_{A,V}^{*}[A_{J}V]$$
(1)

$$\frac{\partial [A_i]}{\partial t} = \nabla \Big[D_A \nabla [A_i] \Big] - k_i^{-} [A_i] [I] + k_i^{+} [A_i] [I] - k_v^{-} [A_i] [V] + k_v^{+} [A_i]$$
(2)

$$\frac{\partial [A_i V]}{\partial t} = \nabla \left[D_{A_i V}^{ch} \{ [V(\Phi)] \} \nabla [A_i] + D_{A_i V}^{*} [A_i] \nabla [V] + \frac{q}{kT} D_{A_i V}^{t} [A_i] \nabla \Phi \right]$$

$$+ k_{\overline{A}} V [A_i] [V] - k_{\overline{A}}^* V [A_i] V$$
(3)

$$\frac{\partial [V]}{\partial t} = D_V \nabla^2 [V] - k_R \left([I] [V] - [I^*] [V^*] \right) - k_{A,V} [A_i] [V] + k_{A,V}^* [A_i V]$$
⁽⁴⁾

$$\frac{\partial [I]}{\partial t} = D_I \nabla^2 [I] - k_R ([I] [V] - [I'] [V'])$$
and the total (chemical) concentration of impurities is

$$A_{T} = \{A_{t}\} + \{A_{t}\} + \{A_{t}V\}$$
(6)

For a list of the used symbols and the method of determination of the Fermi lovel see [5]. This model is currently undergoing computer implementation. The numerical values of the parameters resulting from the analytical calculations (with theoretical physical support) seem to be realistic and they are verified with systematic exportmental data.

We believe that a new generation of diffusion models will be based on a similar set of equations. The major benefit of this approach is that the active concentration is solved during time evolution of the diffusion system and not "after processing" from knowing the chemical concentration.

CONCLUSION

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The ment of an application of process modeling depends on the examiner's viewpoint. Certainly, the contemporary available process modeling tools are sufficient for educational purposes. However, for the design of processes for submicron devices where not only the thermal treatment but also the shape of the structure deturning the diffusion behavior, these tool are still insufficient. Thus a major part of the design phase of new tocnnological processes must still be bead on exportmental work.

In engineering practice, combination of experimental data and simulation is necessary to achieve the acceptable predictability of TCAD tools. For example the module which creates the isolation and bulk of the devices can be characterized almost fully by measurement on big! test objects. Loading of the concentration profile from these measurement into a gnd prepared according to SEM cross-sections we can eliminate errors connected with the epitaxy (aurodoping) and high space changes of structure during high temperature processing. These problems are not traditionally predicted satisfaction by tCAD tools. Even nough we discussed many problems with process modeling, in our opinion the process simulation can contribute to our knowledge of processing phenomena and we can im-

Even though we discussed many problems with process modeling, in our opinion the procuss simulation can contribute to our knowledge of processing phenomena and we can improve our level of understanding of the underlying theory with practical results. Even if we aru not able create the bottor numerical models we can benefit from qualitatively higher level of understanding of our structures. This fact is not negligible

Our discussion was limited to high speed bipolar processes, find-one it is fair to note that the predictability of the simulation results for MOS processes is slightly better than for bipolar processes.

¹⁾ This quantitative estimation of the dependence of the equilibrium concentration of vacances on the doping level is built on a thermodynamic approach applying the neutrol of Lagrangian multiplikers for minimization of the energy of the system. The thermodynamic approach does not show the source of point detects and this leads to inconect conceptualization of the detect likes from or to the surface interface.

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M1, M3, M5 PROCESSING TEMPERATURES

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Fig.1 Simplified diagram of processing temperatures and processing times for processes M1,M2,M3.



Fig.2. Changes in redistribution of impurities after projected thermal budget for NPN transistor



RTA vs FURNACE EXPERIMENT

after projected thermal budget for

N-channel transistor.

Fig.6. Temperature-time profile for anneal of waters in RTA (solid line) and furnace (dotted line)



Fig.4. Diffusion from boron doped polysilicon in rectangular window



Fig.5. Diffusion from boron doped polysilicon in tapered window.



FIg.9. Temperature-time profile for RTA annealing with fast (dotted line) and slow (solid line) cooling rates Fig.10 Active (lower 2 curves) and chemical (upper 2 curves) concentration for fast (dotted line) and slow (solid line) cooling rate during RTA anneal